# High-Pressure Phase Behavior of the Binary System Isobutane + Diamantane 

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#### Abstract

Solid-liquid and vapor-liquid equilibria for the binary system isobutane + diamantane were determined according to the synthetic method in the temperature range (320-530) K and the pressure range (0.310) MPa. Also, the three-phase curve solid diamantane-liquid-vapor was determined. The results show that the slope of this curve demonstrates a discontinuity, which can be explained by the existence of two solid modifications of diamantane. The two branches of this equilibrium intersect at the $\mathrm{S}_{1}-\mathrm{S}_{2}$ equilibrium line of diamantane. The influence of the occurrence of two modifications of diamantane on isobaric solidliquid equilibria is less distinct.


## Introduction

The phase behavior of systems of oil components and diamondoids is important for the recovery of hyperbaric reservoir fluids. The production of these reservoir fluids can be hampered by the precipitation of solid diamondoids such as adamantane or diamantane in pipelines and even in the reservoir.

As a part of a systematic investigation on the phase behavior of light oil components and diamandoids, the highpressure phase behavior of the binary system isobutane + diamantane is determined experimentally. The phase behavior of this binary system is schematically described by Figure 1. Since pure diamantane shows a solid-solid $\left(\mathrm{S}_{1}-\mathrm{S}_{2}\right.$ ) transition line, ${ }^{1}$ the curve representing the solid diamantane-liquid-vapor equilibrium (SLV) splits into two branches. One branch corresponds to the $\mathrm{S}_{1}-\mathrm{L}-\mathrm{V}$ equilibrium, and the other branch corresponds to the $\mathrm{S}_{2}-$ $\mathrm{L}-\mathrm{V}$ equilibrium. Both branches intersect at the $\mathrm{S}_{1}-\mathrm{S}_{2}$ equilibrium line of pure diamantane. The $\mathrm{S}_{1} \mathrm{LV}$ line starts at low temperature in the quadruple point solid methanesolid diamantane-liquid-vapor. The $\mathrm{S}_{2}$ LV line ends at higher temperature in the triple point of pure diamantane. The $S_{1}-S_{2}$ equilibrium line can be constructed using atmospheric data of Reiser et al. ${ }^{1}$ and data for other binary diamantane systems. ${ }^{2}$

## Experimental Section

The experiments were carried out using a so-called Cailletet apparatus. ${ }^{3}$ The top section of a Cailletet tube contains the mixture of isobutane and diamantane. This tube is placed in a thermostat bath filled with silicon oil. The temperature of the silicon oil was kept at a constant temperature within approximately 0.03 K . The temperature was measured with a platinum resistance thermometer (uncertainty $\pm 0.01 \mathrm{~K}$ ), which was calibrated against a secondary standard thermometer. The pressure was measured with a dead weight pressure gauge (Budenberg, uncertainty $\pm 0.003 \mathrm{MPa}$ at pressures below 5 MPa and $\pm 0.01 \mathrm{MPa}$ at higher pressures) or, in case of the measure-

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$T$
Figure 1. $P-T$ projection of the binary system of isobutane (A) and diamantane (B), with a discontinuity in the slope of the SLV equilibrium line at the intersection with the solid-solid transition line of diamantane.


Figure 2. Experimental path taken in order to determine the equilibria.
ments of SLV equilibria, with a manometer (Heise, uncertainty $\pm 0.01 \mathrm{MPa}$ ). The manometer was calibrated against a dead weight gauge.
To measure the $\mathrm{L}-\mathrm{V}$ equilibria, the pressure was gradually increased until the last gas-bubble disappeared (bubble points, line 1 in Figure2) or decreased until the first liquid-


Figure 3. Phase diagrams of $(1-x)$ isobutane $+x$ diamantane at the indicated mole fraction of diamantane.


Figure 4. Isothermal $\mathrm{P}-\mathrm{x}$ cross sections of the $\mathrm{L}-\mathrm{V}$ equilibrium and $P-x$ projection of the SLV equilibria and the critical curve of $(1-x)$ isobutane $+x$ diamantane.
droplet appeared (dew points, line 2 in Figure 2). For the measurements of the $(\mathrm{S}+\mathrm{L}) / \mathrm{L}$ boundary curves, the temperature was, under constant pressure, first decreased until small nuclei appeared. Then the temperature was (gradually) increased until the last crystal dissolved (line 3 in Figure 2).

The $\mathrm{S}-\mathrm{L}-\mathrm{V}$ equilibrium for a binary system has, according to the Gibbs' phase rule, only one degree of freedom. To measure this equilibrium at a fixed temperature, starting from the LV region, the pressure was decreased until solid diamantane was formed and equilibrium was reached (line 4 in Figure 2).

## Materials

The diamantane used during the experiments was obtained from Chevron. To increase the purity, it was sublimated under vacuum. GC analysis showed that the purity was better than 99 mol \%.

Isobutane, or 2-methyl-propane, was supplied by Hoek Loos, with a minimum purity of $99.95 \mathrm{vol} \%$. To check the purity of the isobutane, the vapor pressure was measured from 330 K up to its critical point ( $407.83 \mathrm{~K}, 3.64 \mathrm{MPa}$ ). These experimental results agreed within the experimental accuracy ( $\pm 0.003 \mathrm{MPa}$ ) with the literature data. ${ }^{4}$

## Results

Figure 3 shows a selection of the experimental results. The figure shows $(S+L) \rightarrow L$ and $(L+V) \rightarrow L$ boundary curves for mixtures of constant composition and the threephase curves $S_{1} L V$ and $S_{2} L V$.

Table 1. Vapor-Liquid Equilibria in the System [(1-x) Isobutane + x Diamantane]: Phase Boundaries at Constant Diamantane Mole Fraction x

|  |  | T/K | $\begin{gathered} \mathrm{P} / \\ \mathrm{MPa} \end{gathered}$ | T/K | $\begin{gathered} \mathrm{P} / \\ \mathrm{MPa} \end{gathered}$ | T/K | $\begin{gathered} \mathrm{P} / \\ \mathrm{MPa} \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $x=0.000$ | $\mathrm{L} \rightarrow \mathrm{V}$ | 328.58 | 0.79 | 358.57 | 1.50 | 393.63 | 2.86 |
|  |  | 338.56 | 0.99 | 363.57 | 1.66 | 403.66 | 3.39 |
|  |  | 343.51 | 1.10 | 368.52 | 1.82 | 407.70 | 3.62 |
|  |  | 348.56 | 1.23 | 373.52 | 1.99 | 407.74 | 3.63 |
|  |  | 353.50 | 1.35 | 383.60 | 2.40 |  |  |
| $x=0.030$ | $L \rightarrow L+V$ | 345.23 | 1.099 | 383.13 | 2.271 | 423.81 | 4.211 |
|  |  | 353.18 | 1.296 | 393.13 | 2.687 | 428.13 | 4.409 |
|  |  | 363.17 | 1.578 | 403.11 | 3.151 | 430.58 | 4.515 |
|  |  | 373.12 | 1.902 | 413.10 | 3.657 | 430.88 | 4.527 |
|  | $\mathrm{L}=\mathrm{V}$ | 431.01 | 4.530 |  |  |  |  |
|  | $\mathrm{V} \rightarrow \mathrm{L}+\mathrm{V}$ | 431.13 | 4.537 | 443.29 | 5.05 | 472.02 | 5.82 |
|  |  | 431.29 | 4.545 | 453.20 | 5.40 | 483.05 | 5.94 |
|  |  | 433.33 | 4.631 | 463.11 | 5.69 | 493.04 | 5.86 |
| $x=0.050$ | $L \rightarrow L+V$ | 365.20 | 1.607 | 403.16 | 3.069 | 441.09 | 4.99 |
|  |  | 368.18 | 1.700 | 413.13 | 3.558 | 442.13 | 5.03 |
|  |  | 373.20 | 1.863 | 423.14 | 4.078 | 442.98 | 5.07 |
|  |  | 383.19 | 2.221 | 433.13 | 4.60 |  |  |
|  |  | 393.18 | 2.623 | 439.12 | 4.89 |  |  |
|  | $\mathrm{L}=\mathrm{V}$ | 443.13 | 5.08 |  |  |  |  |
|  | $\mathrm{V} \rightarrow \mathrm{L}+\mathrm{V}$ | 443.23 | 5.09 | 453.15 | 5.55 | 493.11 | 6.86 |
|  |  | 443.61 | 5.10 | 463.10 | 5.98 | 503.09 | 6.94 |
|  |  | 444.09 | 5.13 | 473.13 | 6.37 |  |  |
|  |  | 445.17 | 5.18 | 483.13 | 6.67 |  |  |
| $x=0.101$ | $L \rightarrow L+V$ | 486.07 | 2.229 | 403.34 | 2.940 | 443.40 | 5.00 |
|  |  | 386.65 | 2.252 | 413.33 | 3.404 | 453.33 | 5.54 |
|  |  | 388.49 | 2.325 | 423.33 | 3.905 | 463.45 | 6.06 |
|  |  | 393.37 | 2.518 | 433.37 | 4.443 | 468.28 | 6.30 |
|  | $\mathrm{L}=\mathrm{V}$ | 469.27 | 6.35 |  |  |  |  |
|  | $\mathrm{V} \rightarrow \mathrm{L}+\mathrm{V}$ | 473.38 | 6.54 | 493.91 | 7.44 |  |  |
|  |  | 483.37 | 7.00 | 503.48 | 7.78 |  |  |
| $x=0.198$ | $L \rightarrow L+V$ | 401.67 | 2.682 | 434.00 | 4.184 | 483.92 | 6.92 |
|  |  | 402.64 | 2.722 | 443.99 | 4.670 | 493.89 | 7.41 |
|  |  | 403.92 | 2.772 | 453.87 | 5.25 | 503.90 | 7.86 |
|  |  | 413.96 | 3.208 | 463.87 | 5.83 |  |  |
|  |  | 424.00 | 3.678 | 473.92 | 6.38 |  |  |
| $x=0.313$ | $L \rightarrow L+V$ | 412.53 | 2.910 | 443.77 | 4.282 | 483.57 | 6.25 |
|  |  | 413.64 | 2.958 | 453.90 | 4.775 | 493.56 | 6.75 |
|  |  | 423.74 | 3.377 | 463.94 | 5.271 | 503.48 | 7.22 |
|  |  | 433.74 | 3.813 | 473.87 | 5.77 |  |  |
| $x=0.400$ | $L \rightarrow L+V$ | 421.26 | 2.932 | 453.27 | 4.225 | 493.24 | 5.98 |
|  |  | 423.30 | 3.006 | 463.28 | 4.658 | 503.20 | 6.41 |
|  |  | 433.35 | 3.396 | 473.26 | 5.10 |  |  |
|  |  | 443.29 | 3.804 | 483.25 | 5.55 |  |  |
| $x=0.500$ | $L \rightarrow L+V$ | 433.40 | 2.947 | 463.31 | 3.996 | 493.25 | 5.099 |
|  |  | 443.32 | 3.284 | 473.31 | 4.361 |  |  |
|  |  | 453.29 | 3.636 | 483.32 | 4.731 |  |  |
| $x=0.600$ | $L \rightarrow L+V$ | 438.22 | 2.572 | 463.19 | 3.260 | 493.29 | $4.124$ |
|  |  | 443.34 | 2.713 | 473.20 | 3.546 | 503.30 | 4.421 |
|  |  | 453.44 | 2.994 | 483.23 | 3.841 |  |  |
| $X=0.694$ | $L \rightarrow L+V$ | 453.79 | 2.329 | 473.78 | 2.758 | 503.99 | 3.419 |
|  |  | 458.88 | 2.436 | 483.98 | 2.988 |  |  |
|  |  | 463.74 | 2.537 | 494.00 | 3.198 |  |  |
| $x=0.840$ | $L \rightarrow L+V$ | 482.15 | 1.613 | 493.16 | 1.737 |  |  |
|  |  | 483.17 | 1.623 | 503.26 | 1.852 |  |  |

The plotted SLV data were obtained as described earlier. In principle, the point of intersection of a $(S+L) \rightarrow L$ boundary curve and $a(L+V) \rightarrow L$ boundary curve of the same composition should also yield a SLV point. SLV points determined in this way agree with the directly measured SLV points within the experimental accuracy.

L-V Equilibria. The experimentally determined LV equilibrium points are given in Table 1. The LV equilibrium was measured up to 503 K . Also three critical points were obtained at low diamantane mole fractions. From these data $\mathrm{P}-\mathrm{x}$ cross sections are constructed in Figure 4. Figure 4 also contains the $\mathrm{P}-x$ projection of the composition of the liquid phase along the SLV equilibrium curve and of the binary critical curve $L=V$.

For the lowest composition ( $\mathrm{X}_{\text {diamantane }}=0.030$ ) a liquidvapor transition could no longer be observed at 503 K .

Table 2. Solid-Liquid Equilibria in the System [(1-x) Isobutane + x Diamantane]: Phase Boundaries at Constant Diamantane Mole Fraction $x$

|  | T/K | P/ MPa | T/K | $\begin{gathered} \mathrm{P} / \\ \mathrm{MPa} \end{gathered}$ | T/K | $\begin{gathered} \mathrm{P} / \\ \mathrm{MPa} \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $x=0.030$ | 343.72 | 2.047 | 341.87 | 5.55 | 340.07 | 10.05 |
|  | 343.22 | 3.047 | 341.36 | 7.05 |  |  |
|  | 342.67 | 4.047 | 340.76 | 8.55 |  |  |
| $x=0.050 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 363.90 | 2.045 | 361.20 | 5.54 | 359.41 | 10.04 |
|  | 362.92 | 3.045 | 360.52 | 7.04 |  |  |
|  | 362.08 | 4.045 | 359.92 | 8.54 |  |  |
| $\mathrm{x}=0.101 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 385.58 | 2.218 | 382.88 | 6.05 | 381.60 | 10.05 |
|  | 384.40 | 3.549 | 382.27 | 7.55 |  |  |
|  | 383.87 | 4.549 | 381.78 | 9.05 |  |  |
| $\mathrm{x}=0.198 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 401.22 | 3.051 | 400.59 | 6.05 | 400.44 | 10.05 |
|  | 400.90 | 4.051 | 400.53 | 7.05 |  |  |
|  | 400.73 | 5.05 | 400.44 | 8.55 |  |  |
| $\mathrm{X}=0.313 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 412.66 | 3.047 | 413.05 | 5.647 | 413.76 | 8.55 |
|  | 412.77 | 4.047 | 413.35 | 7.05 | 414.07 | 10.05 |
| $\mathrm{x}=0.400 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 420.33 | 3.049 | 421.26 | 5.549 | 422.46 | 8.55 |
|  | 420.72 | 4.049 | 421.85 | 7.05 | 423.07 | 10.05 |
| $\mathrm{X}=0.500 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 428.88 | 3.048 | 430.28 | 5.55 | 431.73 | 8.55 |
|  | 429.44 | 4.048 | 431.01 | 7.05 | 432.61 | 10.05 |
| $\mathrm{x}=0.600 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{1}$ | 438.07 | 3.050 | 439.54 | 5.55 | 441.53 | 8.55 |
|  | 438.65 | 4.050 | 440.57 | 7.05 | 442.26 | 10.05 |
| $\mathrm{x}=0.694 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{2}$ | 452.13 | 3.048 | 454.15 | 5.55 | 456.54 | 8.55 |
|  | 453.00 | 4.048 | 455.32 | 7.05 | 457.64 | 10.05 |
| $\mathrm{X}=0.840 \mathrm{~L} \rightarrow \mathrm{~L}+\mathrm{S}_{2}$ | 482.30 | 2.051 | 485.87 | 5.55 | 490.33 | 10.05 |
|  | 483.52 | 3.051 | 487.41 | 7.05 |  |  |
|  | 484.48 | 4.051 | 488.89 | 8.55 |  |  |



Figure 5. Solid-liquid solubility curve of $(1-x)$ isobutane $+x$ diamantane at 10 MPa . The dotted line represents the transition temperature, at which diamantane shows a solid-solid transition $\left(\mathrm{S}_{1}-\mathrm{S}_{2}\right)$.
$\mathbf{S}_{\mathbf{1}}$ - $\mathbf{L}$ Equilibria and $\mathbf{S}_{\mathbf{2}}$ - $\mathbf{L}$ Equilibria. The experimental results of the equilibrium-points are given in Table 2. From these data a $\mathrm{T}-\mathrm{x}$ cross section at 10 MPa is constructed in Figure 5. From this figure we observe that at the temperature of the solid-solid transition of pure diamantane also a change in the slope of the liquidus is observed.
$\mathbf{S}_{\mathbf{1}}-\mathbf{L}-\mathbf{V}$ Equilibria and $\mathbf{S}_{\mathbf{2}} \mathbf{- L}-\mathbf{V}$ Equilibria of Isobutane and Diamantane. The experimental results for these equilibria are given in Table 3. The $\mathrm{S}_{1}-\mathrm{L}-\mathrm{V}$ equilibrium line is measured from 320 K up to higher temperatures. As stated in the Introduction; the $\mathrm{S}-\mathrm{L}-\mathrm{V}$ equilibrium line is split into two branches. The experimental data also show that the intersection of these two branches lies at the constructed $\mathrm{S}_{1}-\mathrm{S}_{2}$ equilibrium line. ${ }^{1,2}$ A P -T projection of the experimental results is plotted in Figure 6.

The $\mathrm{P}-\mathrm{x}$ projection of the $\mathrm{S}-\mathrm{L}-\mathrm{V}$ equilibrium was already constructed in Figure 4.

Table 3. Solid Diamantane-Liquid-Vapor Curve in the Binary System Isobutane + Diamantane

| $\mathrm{T} / \mathrm{K}$ | $\mathrm{P} / \mathrm{MPa}$ | $\mathrm{T} / \mathrm{K}$ | $\mathrm{P} / \mathrm{MPa}$ | $\mathrm{T} / \mathrm{K}$ | $\mathrm{P} / \mathrm{MPa}$ | $\mathrm{T} / \mathrm{K}$ | $\mathrm{P} / \mathrm{MPa}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 323.41 | 0.68 | 373.16 | 1.83 | 418.69 | 2.87 | 464.10 | 2.03 |
| 328.35 | 0.76. | 378.16 | 1.98 | 423.34 | 2.86 | 469.10 | 1.91 |
| 333.32 | 0.85 | 379.38 | 2.02 | 428.66 | 2.78 | 474.11 | 1.79 |
| 338.30 | 0.95 | 384.51 | 2.19 | 433.40 | 2.67 | 478.97 | 1.63 |
| 343.28 | 1.06 | 389.35 | 2.33 | 438.87 | 2.49 | 483.87 | 1.47 |
| 348.27 | 1.17 | 393.33 | 2.45 | 443.67 | 2.36 | 488.01 | 1.33 |
| 353.28 | 1.29 | 398.33 | 2.58 | 448.38 | 2.32 | 492.95 | 1.14 |
| 358.27 | 1.43 | 403.34 | 2.70 | 448.61 | 2.30 | 498.02 | 0.94 |
| 363.26 | 1.55 | 408.34 | 2.78 | 453.96 | 2.23 | 503.03 | 0.73 |
| 368.32 | 1.69 | 413.31 | 2.85 | 458.88 | 2.14 | 517.65 | 0.05 |



Figure 6. Three-phase equilibria of isobutane + diamantane. Also, the phase equilibrium lines of pure diamantane are presented in this figure. ${ }^{1,2}$

## Conclusions

The binary system of isobutane and diamantane shows a discontinuity in the slope of the SLV equilibrium line. This line is split into two sections: an $\mathrm{S}_{1} \mathrm{LV}$ and $\mathrm{S}_{2} \mathrm{LV}$ equilibrium line. These lines intersect at the $S_{1}-S_{2}$ equilibrium line of pure diamantane which was constructed from previous measurements on other binary systems of diamantane. Also, the isobaric $T-x$ cross section at 10 MPa for the solid-liquid equilibria shows a change in slope at the solid-solid transition temperature of diamantane.

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## Literature Cited

(1) Reiser, J.; McGregor, E.; J ones, J.; Enick, R.; Holder, G. Adamantane and Diamantane; Phase Diagrams, Solubilities, and Rates of Dissolution. Fluid Phase Equilib. 1996, 117, 160-170.
(2) de Loos, Th. W.; Poot, W. To be published.
(3) de Loos, Th. W.; van der Kooi, H. J.; Ott, P. L. Vapour + Liquid Equilibria in the System Ethane + 2-Methylpropane. J. Chem. Eng. Data 1986, 31, 166-168.
(4) Vargaftik, N. B.; Vinogradov, Y. K.; Yargin, V. S. Handbook of Physical Properties of Liquids and Gases, 3rd ed.; Begell House Inc.: New York, 1999.

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